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T.E. (Mechanical/Mechanical Sandwich) HEAT AND MASS TRANSFER (2019 Rattern) (Semester - I) (302042)

Time: 2½ Hours] [Max. Marks: 70

Instructions to the candidates:

- 1) Solve Q1 or Q2, Q3 or Q4, Q5 or Q6, Q7 or Q8.
- 2) Neat diagrams must be drawn wherever necessary.
- 3) Figures to the right side indicate full marks.
- 4) Use of Calculator is allowed.
- 5) Assume Suitable data if necessary.
- Q1) a) A vertical plate is maintained at 40°C in 20°C still air. Determine the height at which the boundary layer will turn turbulent if turbulence sets in at A Gr. Pr = 10°. Repeat the problem for water flow at film temperature of 30°C. Comment on the results of solution.
 - b) Explain in brief (Any two)

[8]

- i) Local and average Heat Transfer coefficient
- ii) Hydrodynamic and Thermalboundary layer
- iii) Critical Heat Flux
- iv) Significance of any 2 non dimensionless numbers

OR

- Q2) a) Explain the types of boiling and pool boiling phenomenon in detail with neat sketch of boiling curve. [8]
 - b) Air at atmospheric pressure and 40°C flows with velocity of U = 5 m/sec over a 2 m long flat plate whose surface is kept at a uniform temperature of 120°C. Determine the average heat transfer coefficient over 2 m length of plate. Also determine the rate of heat transfer between the plate and air per 1 m width of plate (Air at 1 atm. And 80°C, v = 2.107 × 10⁵ m²/sec, k = 0.03025 W/mk, Pr = 0.695). [9]
- Q3) a) The energy received from the sun at the earth's atmosphere has been measured as 1353 W/m^2 . The diameter of the earth = $1.29 \times 10^7 \text{m}$. Diameter of the sun = $1.39 \times 10^9 \text{ m}$. Mean distance = $1.5 \times 10^{11} \text{m}$. Estimate the emissive power of the sun and the surface temperature assuming it to be black. Assuming that the source of energy for the earth is from the sun and earth to be black, estimate the temperature of the earth. [8]

P.T.O.

b)	Exp	plain in brief	[10]
	i)	Kirchoffs Law	
	ii)	Stefan Boltzmans law	
	iii)	Wiens Displacement law	
	iv)	Shape Factor	
	v)	Electrical analogy for radiation	
		OR	
a)	Two	o large parallel plates with $\epsilon = 0.5$ each are maintained at diff	erent
		nperatures and are exchanging heat only by radiation. Two eq	_
	- X.	geradiation shields with surface emissivity 0.05 are introduced in pa	
	toti	he plates; find the percentage reduction in net radiative heat tran	nster. [10]
b)	Def	fine shape factor algebra and explain any 4 sabent features of s	
0)	fact		[8]
a)	Ēxp	olain Fick's law for mass diffusion	[8]
b) \	The	e molecular weights of the two components A and B of a gas mi	xture
		24 and 28 respectively. The molecular weight of gas mixture is f	
		be 30. If the mass concentration of the mixture is 1.2 kgm ³ , deter	
	the	following	[9]
	i)	Molar fractions	
	ii)	Mass fractions	
	iii)	Total pressure if temperature of mixture is 290K	ري:
		OR	
a)	_		term
	con	servation of species.	[8]
b)		drogen gas is maintained at pressure of 2.4 bars and 1 bar on opp	
		es of a plastic membrane 0.3 mm thick. The binary diffusion coeff hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and solubility of hydrogen in the plastic is 8.6×10^{-8} m ² /s and $8.6 \times 10^{-$	
~		the membrane is 0.00145 kg mole/m ³ -bar. (molecular weight of hydrone)	_
		kg/kg mole)	- 6
	Cal	culate under uniform conditions of 24°C, the following:	[9]
	i)	Molar concentration of hydrogen at opposite face of membra	ine
	ii)	Molar and mass diffusion of hydrogen through membrane	
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Q4)

Q5)

Q6)

b) In a double pipe heat exchanger hot water flows at the rate of 5000kg/h and gets cooled from 95°C to 65°C. At the same time 50000kg/h of cooling water at 30°C enters heat exchanger. The flow conditions are such that overall heat transfer coefficient remains constant at 2270 W/m²K. Determine the heat transfer area required and the effectiveness, assuming two streams are in parallel flow. Assume for both the streams $C_p = 4.2 \text{ kJ/kgK}$. [10]

OR

Q8) a) Derive LMTD for Counter flow heat exchanger.

[8]

b) A counter flow double pipe heat exchanger uses superheated steam to heat water at the rate of 10500kg/h. The steam enters the heat exchanger at 180°C and leaves at 130°C. The inlet and exit temperatures of water are 30°C and 80°C, If the overall heat transfer coefficient from steam to water is 814 W/m²⁰C. Calculate the heat transfer area. What would be the increase in area if the fluid passes are in parallel? [10]

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